



Research article

Study of Corrosion and Corrosion Protection of Stainless steel in Phosphate Fertilizer Industry

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Abstract

Phosphate industries use bulk amount of conc. H_2SO_4 during production of phosphate fertilizers. Stainless steel is major supporting metal for completion for several processing operational works. This acid produces corrosive effect for stainless steel. It develops corrosion cell on the surface of base metal and it changes its internal morphology as well as physical, chemical, mechanical properties. H_2SO_4 behaves like diabetes for this industrial metal and industries face economical. Industries expense huge money for repairing and maintenance works and sometimes production work stopped and major accident occurs. This is vital setback for industries. The eradication of corrosion problems used organic inhibitors like 1-(2-chlorophenyl)methanamine and 1-(2-bromophenyl)methanamine and its inhibition effect and surface coverage area studied at different temperatures 333^0K , 343^0K and 353^0K in presence of 15% H_2SO_4 and 15mM concentrations of inhibitors. The corrosion rate of metal determined absence and presence of inhibitors by weight loss experiment and potentiostat techniques. The surface adsorption phenomenon, surface thin film and complex formation by inhibitors were analyzed by application of activation energy, heat of adsorption, free energy, enthalpy and entropy. Analysis of all experimental works the used inhibitors produced anticorrosive effect in H_2SO_4 acidic medium. **Copyright © AJESTR, all rights reserved.**

Keywords: Stainless steel, inhibitors, weight loss, potentiostat, surface coverage area.

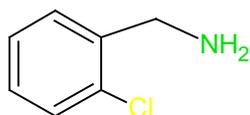
Introduction

The Corrosion of protection of metal is a bigger issue among the corrosion scientists and researchers. It is not fully control but its effect can be minimized by suitable remedies e.g. give proper design and shape of operational metals[1], take care of operating temperatures and surrounding atmosphere [2], applied different types of coatings [3], using cathodic and anodic protection [4] and addition of inhibitors[5]. Operational equipments were not designed well manner [6] then it created corrosion problems like galvanic, pitting crevice, stressed, intergranular, blistering, embrittlement in presence of corrosive atmosphere. Coatings is major tools for corrosion alleviation of metal. It applied as metallic coating [7], inorganic coating [8], organic coating [9], painting coating, polymeric coating, and nanocoatings [10]. These coating did not provide good support for metal in acidic environment because porosities were developed on the surface of base metal during coatings and H^+ ions entered into porosities of coating materials in this ways generated corrosion cell and deteriorating coating materials. Inhibitors action can be checked corrosion in acidic medium which are inorganic, organic and mixed types inhibitors. Organic inhibitors possessed nitrogen, oxygen, sulphur, silicon, phosphorous, methyl, phenyl, primary, secondary and tertiary alkyl groups; they are highly electron rich organic compounds which produce adsorption effect on surface of metal. They can be adsorbed on the surface of base metals by physical-chemical adsorption. These organic compounds above mentioned functional groups have high electronic charge density; they received H^+ ions and suppress the attacking speed of hydrogen ions. They have capability to form thin film and complexed compound with metal and control aggressiveness of H^+ ions. Aromatic and heterocyclic organic compounds containing above mentioned functional groups produced anticorrosive effect in acidic medium. Nanocoating of $Zn_3(PO_4)_2$ [11], $Mg_3(PO_4)_2$ [12] and $AlPO_4$ [13] in presence of DLC (diamond like carbon) controlled high temperatures corrosion and minimize hydrogen ions attack. Plasma coating gave corrosion protection of metal in acidic environment. Composite coating materials have anticorrosive character in hostile environment. The above mentioned artificial inhibitors and coating materials are not beneficial for environment so new a day's researchers used natural organic inhibitors for corrosion control. Aloe Vera used an inhibitor for corrosion protection storage can of beverage [14], milk [15], orange juice [16] and vegetables [17].

Experimental procedure

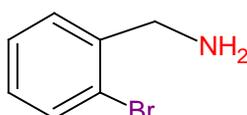
Stainless steel coupons were cut into size of $(5 \times 3) \text{ cm}^2$. Its surface was rubbed with emery paper and samples were washed with double distilled water. Finally it was rinsed with acetone and dried with air dryer and kept into desiccator. Test sample dipped into 250ml biker with support glass hook and corrosion rate metal determined absence and presence of inhibitors 1-(2-chlorophenyl)methanamine and 1-(2-bromophenyl)methanamine at different temperatures 333^0K , 343^0K and 353^0K and 15mM concentration. Thermostat used take corrosion rate results for above mention temperature. The corrosion rate was measured by gravimetric method.

The corrosion current density and corrosion rate without and with inhibitors were calculated bypotentiostatic polarization technique with help of an EG & G Princeton Applied Research Model 173 Potentiostat. A platinum electrode was used as an auxiliary electrode and a calomel electrode was used as reference electrode with stainlesssteel coupons.



1-(2-chlorophenyl)methanamine

IH(I)



1-(2-bromophenyl)methanamine

IH(II)



Results and Discussion

The corrosion rates of stainless steel without and with inhibitors 1-(2-chlorophenyl)methanamine and 1-(2-bromophenyl) methanamine were determined by equation 1 in 10% H₂SO₄ solution and its results were mentioned in Table 1.

$$K \text{ (mmpy)} = 87.6 W / D A t \quad (1)$$

where W = weight loss of test coupon expressed in gm, A = Area of test coupon in square centimeter, D = Density of the material in g/cm³.

The surface coverage areas (θ) and the inhibition efficiencies (IE) occupied by inhibitors were calculated equation 2 and 3 and their results were written in Table 1.

$$\theta = (1 - K / K_0) \quad (2)$$

where θ = Surface coverage area, K₀ = corrosion rate without inhibitor, K = corrosion rate with inhibitor

$$IE = (1 - K / K_0) \times 100 \quad (3)$$

where K₀ is the corrosion rate without inhibitor, K = corrosion rate with inhibitor

The corrosion rate, surface coverage area and inhibition efficiency were calculated by equation 1, equation 2 and equation 3 in at different temperatures and 15mM concentration of inhibitors, its values were mentioned in Table 1. The results of Table 1 observed corrosion rate increased in acidic medium without addition of inhibitors but its values decreased after addition of addition of inhibitors. The results of surface coverage area and inhibition efficiency with 1-(2-chlorophenyl)methanamine and 1-(2-bromophenyl)methanamine enhanced at different temperatures and it looked in figure 1 (surface coverage area) versus T⁰K and figure 2 IE (inhibition efficiency) versus T⁰K.

Table 1: Corrosion of stainless steel in different temperatures without and with inhibitors in 15% H₂SO₄

Inhibitors	Temperatures	333 ⁰ K	343 ⁰ K	353 ⁰ K	C (m M)
IH(0)	K ₀	391	565	836	00
	logK ₀	2.592	2.752	2.922	
IH(I)	K	118	192	230	15
	logK	2.071	2.283	2.518	
	log($\theta/1-\theta$)	0.363	0.290	0.185	
	θ	0.698	0.661	0.605	
	IE (%)	69.80	66.10	60.50	
IH(II)	K	61	155	201	15
	logK	1.785	2.191	2.303	
	log($\theta/1-\theta$)	0.729	0.421	0.498	
	θ	0.843	0.725	0.759	
	IE (%)	84.30	72.50	75.90	

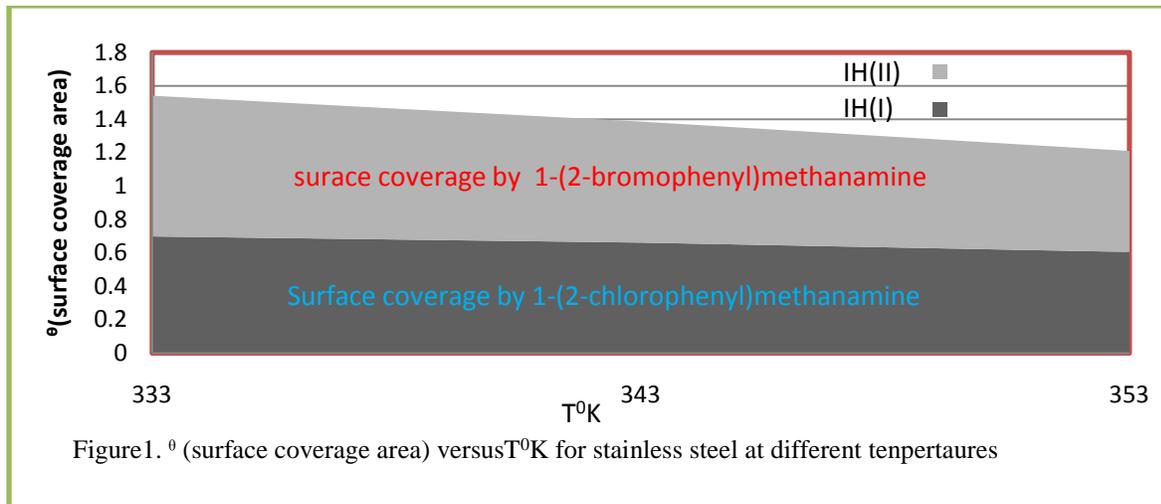


Figure1. ° (surface coverage area) versus T°K for stainless steel at different temperatures

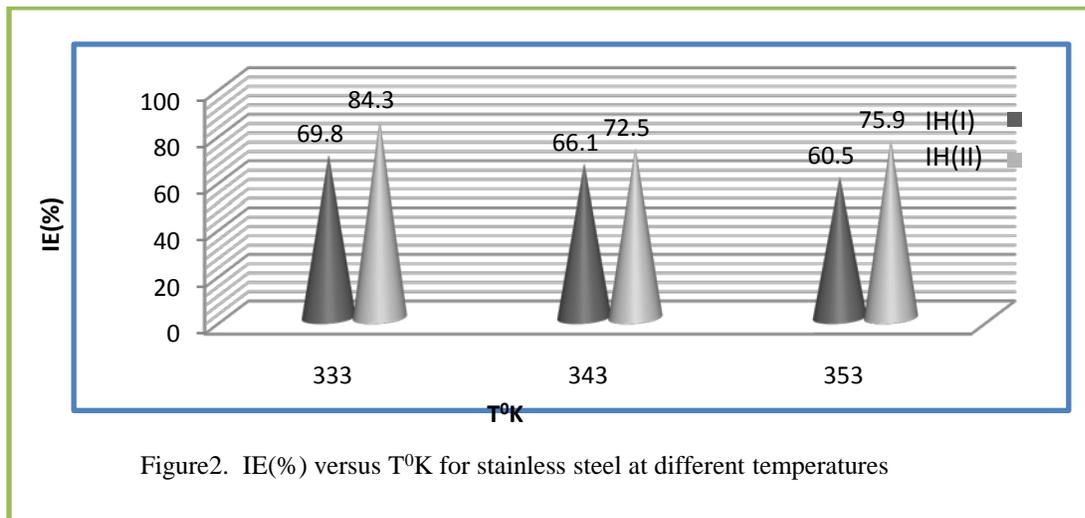


Figure2. IE(%) versus T°K for stainless steel at different temperatures

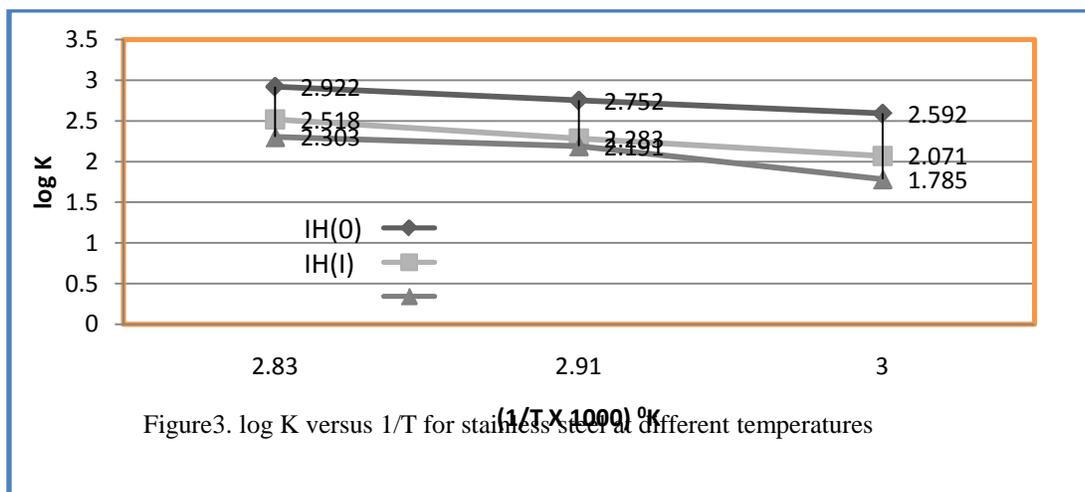


Figure3. log K versus 1/T for stainless steel at different temperatures



The activation energy, heat of adsorption, free energy, enthalpy and entropy for inhibitors 1-(2-chlorophenyl)methaneamine and 1-(2-bromophenyl)methaneamine were calculated by equation4, equation5, equation6 and equation7 and their values were recorded in Table2. The activation energy increased without inhibitors and its values decreased with inhibitors. It indicated that inhibitors bonded with base metal. Heat of adsorption negative sign noticed that inhibitors adhered with metal by physical adsorption and its plot between $\log(\theta/1-\theta)$ versus $1/T$ looked in figure4. The results of free energy, enthalpy and entropy values were shown negative sign which depicted that adsorption occurred on the surface of metal and the graph of all thermodynamical values ($E_a, Q_{ads}, \Delta G, \Delta H$ and ΔS) versus θ (surface coverage area) were presented in figure5 .

$$d/dt (\log K) = E_a / R T^2 \quad (4)$$

where T is temperature in Kelvin and E_a is the activation energy

$$\log (\theta / 1-\theta) = \log (A .C) - (Q_{ads} / R T) \quad (5)$$

where T is temperature in Kelvin and Q_{ads} , heat of adsorption

$$\Delta G = -2.303RT [\log C - \log (\theta/1-\theta) + 1.72] \quad (6)$$

where T is temperature in Kelvin and ΔG free energy

$$K = R T / N h \log (\Delta S^\# / R) X \log (-\Delta H^\# / R T) \quad (7)$$

where N is Avogadro's constant, h is Planck's constant, $\Delta S^\#$ is the change of entropy activation and $\Delta H^\#$ is the change of enthalpy activation.

Table2. Thermodynamical values of inhibitors in 15% H_2SO_4 for stainless steel

Inhibitors	Temperatures	333 ⁰ K	343 ⁰ K	353 ⁰ K
IH(0)	$E_a(o)(kJmol^{-1})$	148	153	157
IH(I)	$E_a(kJmol^{-1})$	118	126	134
	$Q_{ads.}(kJmol^{-1})$	-21	-16	-10
	$\Delta G(kJmol^{-1})$	-206	-211	-216
	$\Delta H(kJmol^{-1})$	-92	-101	-206
	$\Delta S(JK^{-1})$	-99	-108	-117
IH(II)	$E_a(kJmol^{-1})$	102	117	123
	$Q_{ads.}(kJmol^{-1})$	-42	-23	-26
	$\Delta G(kJmol^{-1})$	-189	-205	-204
	$\Delta H(kJmol^{-1})$	-75	-96	-99
	$\Delta S(JK^{-1})$	-88	-104	-109

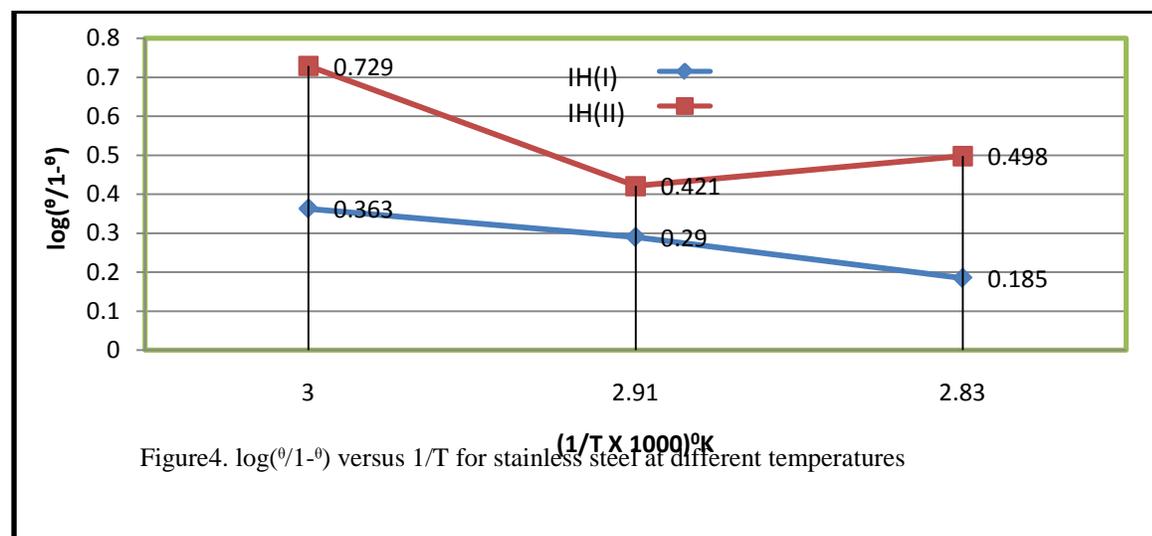
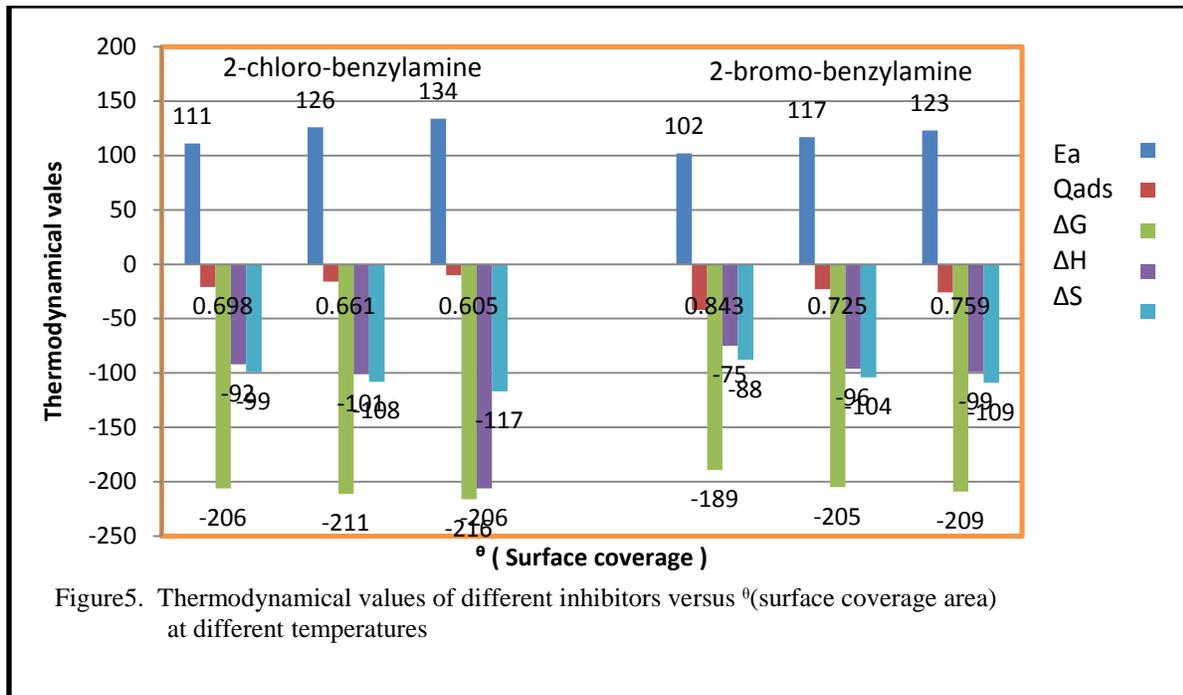


Figure4. $\log(\theta/1-\theta)$ versus $1/T$ for stainless steel at different temperatures



The corrosion current density determined in the absence and presence of inhibitor with the help of equation 8 and their values were recorded in Table 3.

$$\Delta E/\Delta I = \beta_a \beta_c / 2.303 I_{\text{corr}} (\beta_a + \beta_c) \quad (8)$$

where $\Delta E/\Delta I$ is the slope which linear polarization resistance (R_p), β_a and β_c are anodic and cathodic Tafel slope respectively and I_{corr} is the corrosion current density in mA/cm^2 .

The metal penetration rate (mmpy) was determined by equation 9 in absence and presence of inhibitors.

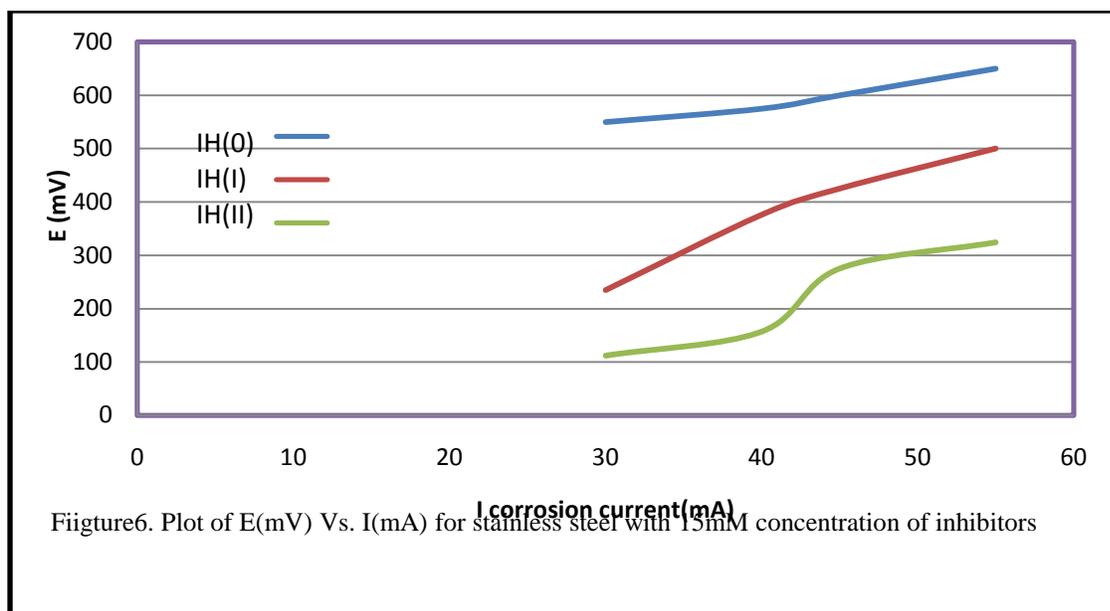
$$C. R (\text{mmpy}) = 0.327 I_{\text{corr}} (\text{mA}/\text{cm}^2) \times \text{Eq. Wt} (\text{g}) / \rho (\text{g}/\text{cm}^3) \quad (9)$$

where I_{corr} is the corrosion current density ρ is specimen density and Eq. Wt is specimen equivalent weight.

The results of Table 3 indicated that corrosion current increase without inhibitors and its values reduced after addition of inhibitors because these inhibitors enhanced cathodic current so corrosion current and corrosion rate minimized. Tafel graph was plotted in Figure 6 between electrode potential and corrosion current density in the absence and presence of inhibitors.

Table 3. Potentiostatic polarization of inhibitors in 15mM concentration and 15% of H_2SO_4

$\Delta E(\text{mV})$	ΔI	β_a	β_c	$I_{\text{corr}}(\text{mA}/\text{cm}^2)$	$K(\text{mmpy})$	$C(\text{mM})$
-650	550	350	250	55.79	4.379	0.00
-600	475	225	315	45.17	0.354	15
-575	350	175	325	30.10	0.236	



Conclusion:

These inhibitors possessed electron releasing functional which has capability to enhance electron charge density towards corroded metal and protected base metal. The results of surface coverage area and inhibition efficiency with both inhibitors indicated that a protective layer developed on the surface of metal. The results of activation energy, heat of adsorption, free energy, enthalpy and entropy were shown both inhibitors bonded with base metal physical-chemical adsorption.

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